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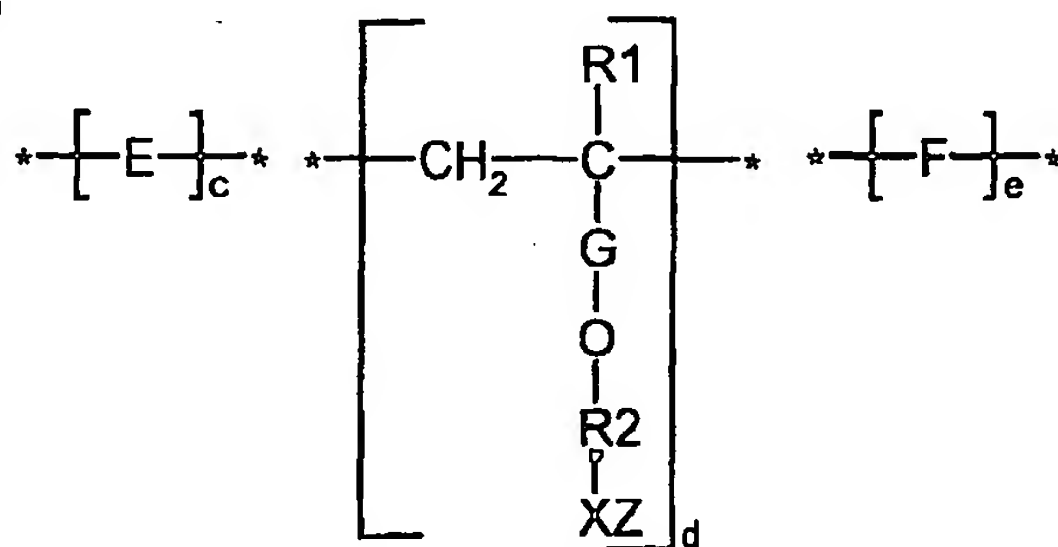
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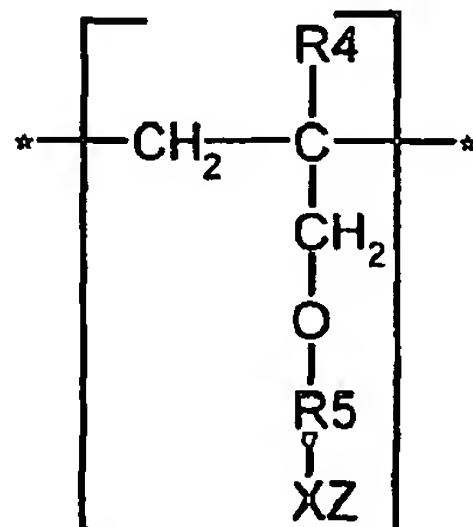
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(54) Title: METHOD FOR CONTROLLONG SCALE FORMATION AND DEPOSITION IN AQUEOUS SYSTEMS

(I)



(II)



(57) Abstract: Novel water-soluble or water-dispersible polymers useful for inhibiting the formation and deposition of scale forming moieties in aqueous systems comprising repeat units characterized by the Formula I: R1 | *--[-E-]c--*[-CH2-C-]d-*[-F-]e-* | G | O | R2 | XZ Wherein E is the repeat unit remaining after polymerization of an ethylenically unsaturated compound; preferably, a carboxylic acid, sulfonic acid, phosphonic acid, or amide form thereof or mixtures thereof. R1 is H or lower (C1-C4) alkyl. G is -CH2- or -CHCH3-; R2 is -(CH2-CH2-O)n- or -(CH2-CHCH3-O)m- where n and m range from about 1 to 100, preferably n is greater than 10 and m ranges from about 1 to 20. X is an anionic radical selected from the group consisting of SO3, PO3, or COO; Z is H or hydrogens or any water soluble cationic moiety which counterbalances the valence of the anionic radical X, including but not limited to Na, K, Ca, or NH4. F, when present, is a repeat unit having the structure of Formula II: R4 | *[-CH2-C-]* | CH2 | O | R5 | XZ wherein X and Z are the same as in Formula I. R4 is H or lower (C1-C4) alkyl. R5 is hydroxy substituted alkyl or alkylene having from about 1 to 6 carbon atoms.



Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM),
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GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent
(BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR,
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METHOD FOR CONTROLLING SCALE FORMATION AND DEPOSITION IN AQUEOUS SYSTEMS

FIELD OF THE INVENTION

The present invention relates to novel polymeric compositions and their use in methods of inhibiting corrosion and controlling the formation and deposition of scale imparting compounds in aqueous systems such as cooling, boiler and gas scrubbing systems; pulp and paper manufacturing processes; in the pretreatment of metals; as rheology modifiers for concrete and cement additives; as cleaning agents for membranes; and as hydrophilic modifier components in personal care, cosmetic and pharmaceutical formulations. The novel polymeric compositions which are useful in accordance with the present invention comprise water-soluble or water-dispersible copolymers of ethylenically unsaturated monomers with sulfate, phosphate, phosphite or carboxylic terminated polyalkylene oxide allyl ethers.

BACKGROUND OF THE INVENTION

The problems of corrosion and scale formation and the attendant effects have troubled water systems for years. For instance, scale tends to accumulate on internal walls of various water systems, such as boiler and cooling systems, and thereby materially lessen the operational efficiency of the system.

Deposits in lines, heat exchange equipment, etc., may originate from several causes. For example, precipitation of calcium carbonate, calcium sulfate and calcium phosphate in the water system leads to an accumulation of these scale-imparting compounds along or around the metals' surfaces which contact the flowing water circulating through the system. In this manner, heat transfer functions of the particular system are severely impeded.

Corrosion, on the other hand, is a degradative electrochemical reaction of a metal with its environment. Simply stated, it is the reversion of refined metals to their natural state. For example, iron ore is iron oxide. Iron ore is refined into

steel. When steel corrodes, it forms iron oxide which, if unattended, may result in failure or destruction of the metal, causing the particular water system to shut down until the necessary repairs can be made.

Typically, in cooling water systems, the formation of calcium sulfate,
5 calcium phosphate and calcium carbonate, among others, has proven deleterious to the overall efficiency of the cooling water system. Recently, due to the popularity of cooling treatments using high levels of orthophosphate to promote passivation of the metal surfaces in contact with the system water, it has become critically important to control calcium phosphate crystallization so that relatively
10 high levels of orthophosphate may be maintained in the system to achieve the desired passivation without resulting in fouling or impeded heat transfer functions which would normally be caused by calcium phosphate deposition.

Silica (SiO_2) is present in most natural waters. When these waters are cycled in a cooling tower, the silica level increases and often a level is reached where
15 precipitation of a silica species occurs. Sometimes the precipitation proceeds by the polymerization of silica itself, resulting in a silica gel. For this to occur, a relatively high SiO_2 concentration is required, usually greater than approximately 200 ppm. However, when certain cations are present, silica species can precipitate at much lower concentrations. Cations that promote silica
20 precipitation include, but are not limited to, Al^{3+} , Mg^{2+} , Zn^{2+} and Fe^{3+} . Aluminum is very insoluble in water and readily precipitates under cooling water conditions. When aluminum gets into a cooling system (such as by carryover) it can cause serious precipitation problems. One such problem is the precipitation of phosphate species which may be present as a corrosion inhibitor. Such
25 precipitates can be problematic due to both deposition and corrosion effects.

Although steam generating systems are somewhat different from cooling systems, they share a common problem in regard to deposit formation.

As detailed in the Betz Handbook of Industrial Water Conditioning, 9th Edition, 1991, Betz Laboratories Inc., Trevose, Pa, Pages 96-104, the formation

of scale and sludge deposits on boiler heating surfaces is a serious problem encountered in steam generation. Although current industrial steam producing systems make use of sophisticated external treatments of the boiler feedwater, e.g., coagulation, filtration, softening of water prior to its feed into the boiler system, these operations are only moderately effective. In all cases, external treatment does not in itself provide adequate treatment since muds, sludge and hardness-imparting ions escape the treatment, and eventually are introduced into the steam generating system.

In addition to the problems caused by mud, sludge or silt, the industry has also had to contend with boiler scale. Although external treatment is utilized specifically in an attempt to remove calcium and magnesium from the feedwater, scale formation due to residual hardness, i.e., calcium and magnesium salts, is always experienced. Accordingly, internal treatment, i.e., treatment of the water fed to the system, is necessary to prevent, reduce and/or retard formation of scale imparting compounds and their resultant deposition. In addition to carbonates of magnesium and calcium being a problem as regards scale, having high concentrations of phosphate, sulfate and silicate ions either occurring naturally or added for other purposes cause problems since calcium and magnesium, and any iron or copper present, react and deposit as boiler scale. As is obvious, the deposition of scale on the structural parts of a steam generating system causes poorer circulation and lower heat transfer capacity, resulting in an overall loss in efficiency.

RELATED ART

U. S. Patent No. 4,471,100 to Tsubakimoto et al. discloses a copolymer consisting of maleic acid and polyalkyleneglycol monoallyl ether repeat units useful as a dispersant for cement and paint and as a scale inhibitor for calcium carbonate.

U. S. Patents Nos. 5,180,498; 5,292,379; and 5,391,238 to Chen et al.,

disclose copolymers of acrylic acid and polyethyleneglycol allyl ether for boiler water treatment and metal pretreating applications.

U. S. Patent No. 5, 362,324 describes terpolymers of (meth) acrylic acid and polyethyleneglycol-monomethylether-(meth) acrylate and
5 polypropyleneglycol di(meth)acrylate for superplasticizer applications. U. S. Patent No. 5,661, 206 and EP448717 disclose similar technology but using diepoxy based compounds as crosslinking agents. Japanese Patents 93660, 226757 and 212152 disclose acrylic acid terpolymers with sodium
methallylsulfonate and methoxy polyethylene glycol-monomethacrylate for
10 superplasticizer applications.

U. S. Patent No. 5,575,920 to Freese et al. discloses terpolymers of acrylic acid, allyloxy-2-hydroxypropylsulfonic ester (AHPS) and polyethyleneglycol allyl ether for cooling water treatment as calcium phosphate inhibitors.

15 U. S. Patent No. 3,875,202 to Steckler discloses polymerizable ammonium and alkali metal salts of sulfated monoethylenically unsaturated alcohols of from 3 to 12 carbon atoms and of the alkenoxylated adducts of such alcohols. The polymerizable monomers are useful as co-polymerizable surfactants for self-stabilizing latexes and as comonomers in the
20 copolymerization with other monomers in the preparation of co- or ter-polymeric films and fibers, especially as receptors for basic dyes and to build in anti-static properties. Monomers such as vinyl chloride, ethyl acrylate, 2-ethylhexyl acrylate, vinyl acetate and N-methyl acrylamide are disclosed in the patent to be copolymerizable with the ammonium salt of sulfated monoethylenically
25 unsaturated alcohols. The copolymers disclosed are not water-soluble.

U. S. Patent No. 5,705,665 to Ichinohe et al. relates to organic silicon compounds having as one of the components ethoxylated allyl alcohol with alkali metal salt of sulfonate group in the molecule. The resulting compound is useful

as a surface treating agent and modifier for inorganic material. The copolymers disclosed are not water-soluble or dispersible.

DETAILED DESCRIPTION OF THE INVENTION

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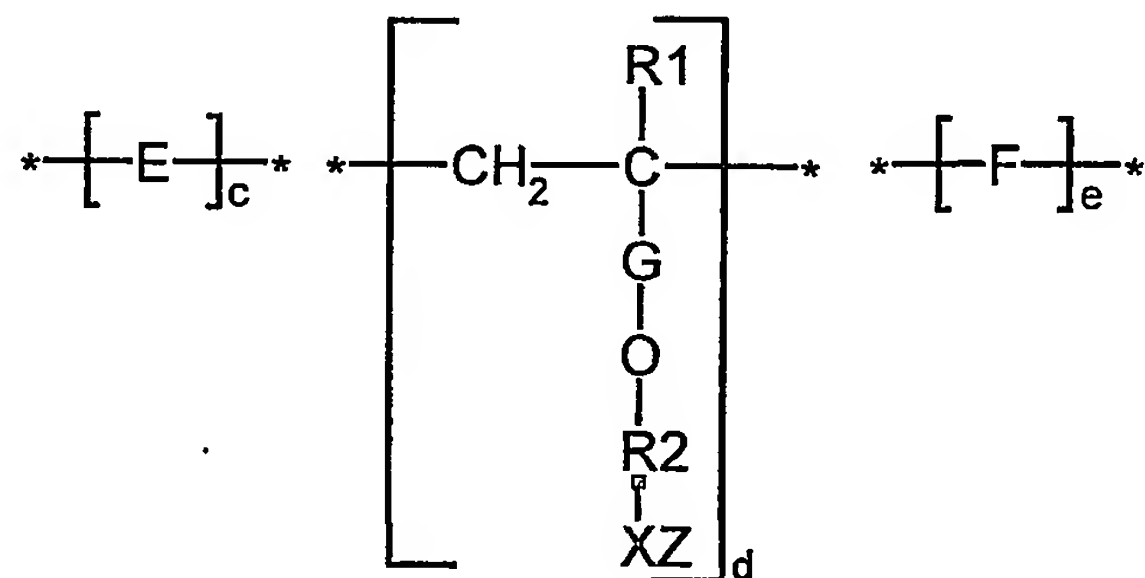
The present invention pertains to novel water-soluble or water dispersible polymers, which contain pendant functional groups and their use in controlling the formation and deposition of mineral deposits and in inhibiting corrosion in various aqueous systems. The novel polymers useful in the present invention are

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copolymers or terpolymers having the structure of Formula I.

Formula I

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Wherein E is the repeat unit remaining after polymerization of an ethylenically unsaturated compound; preferably, a carboxylic acid, sulfonic acid, phosphonic acid, or amide form thereof or mixtures thereof. R₁ is H or lower (C₁-C₄) alkyl. G is -CH₂- or -CHCH₃-; R₂ is -(CH₂-CH₂-O)_n or -(CH₂-CHCH₃-O)_m where n and m range from about 1 to 100, preferably n is greater than 10 and m ranges from about 1 to 20. X is an anionic radical selected from the group consisting of SO₃, PO₃, or COO; Z is H or hydrogens or any water

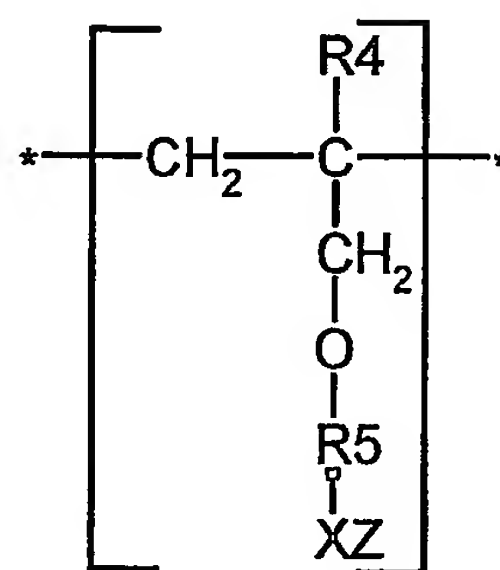
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soluble cationic moiety which counterbalances the valence of the anionic radical

X, including but not limited to Na, K, Ca, or NH_4 . F, when present, is a repeat unit having the structure of Formula II.

Formula II

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In Formula II, X and Z are the same as in Formula I. R_4 is H or lower ($\text{C}_1\text{--C}_4$) alkyl. R_5 is hydroxy substituted alkyl or alkylene having from about 1 to 6 carbon atoms.

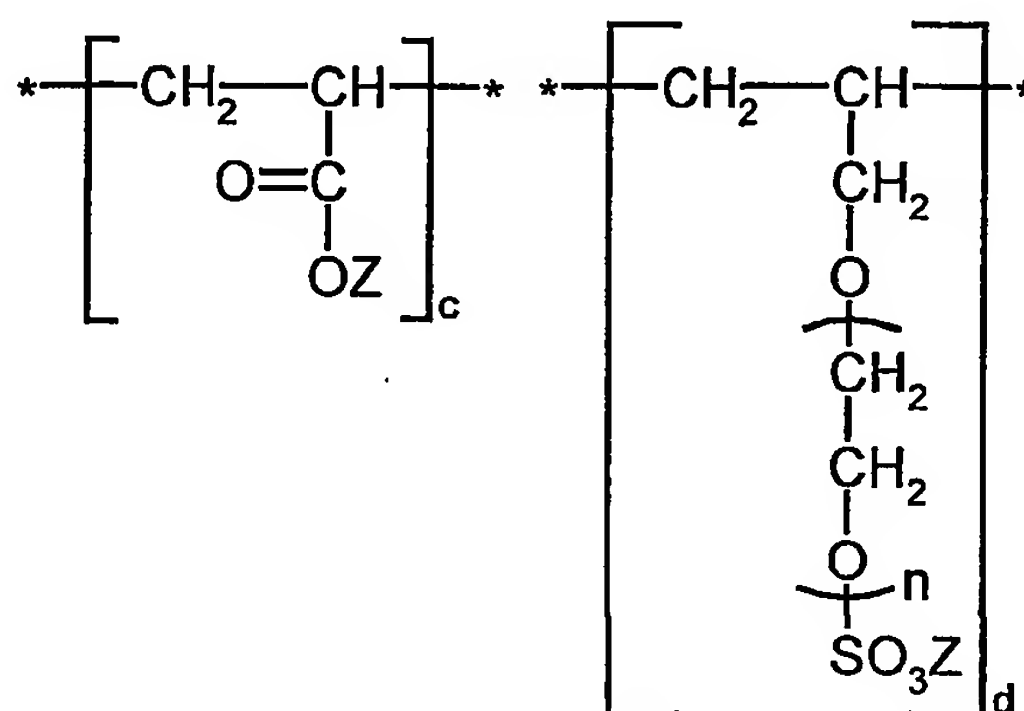
With respect to E of Formula I, it may comprise the repeat unit obtained
 15 after polymerization of a carboxylic acid, sulfonic acid, phosphonic acid, or amide form thereof or mixtures thereof. Exemplary compounds include but are not limited to the repeat unit remaining after polymerization of acrylic acid, methacrylic acid, acrylamide, methacrylamide, N-methyl acrylamide, N, N-dimethyl acrylamide, N-isopropylacrylamide, maleic acid or anhydride, fumaric
 20 acid, itaconic acid, styrene sulfonic acid, vinyl sulfonic acid, isopropenyl phosphonic acid, vinyl phosphonic acid, vinylidene di-phosphonic acid, 2-acrylamido-2-methylpropane sulfonic acid and the like and mixtures thereof. Water-soluble salt forms of these acids are also within the purview of the present invention. More than one type of monomer unit E may be present in the polymer
 25 of the present invention.

Subscripts c, d, and e in Formula I are the molar ratio of the monomer repeating unit. The ratio is not critical to the present invention providing that the resulting copolymer is water-soluble or water-dispersible. Subscripts c and d are positive integers while subscript e is a non-negative integer. That is, c and d are integers of 1 or more while e can be 0, 1, 2...etc.

A preferred copolymer of the present invention, that is where $e = 0$, is acrylic acid/polyethyleneglycol monoallyl ether sulfate of the structure:

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Formula III



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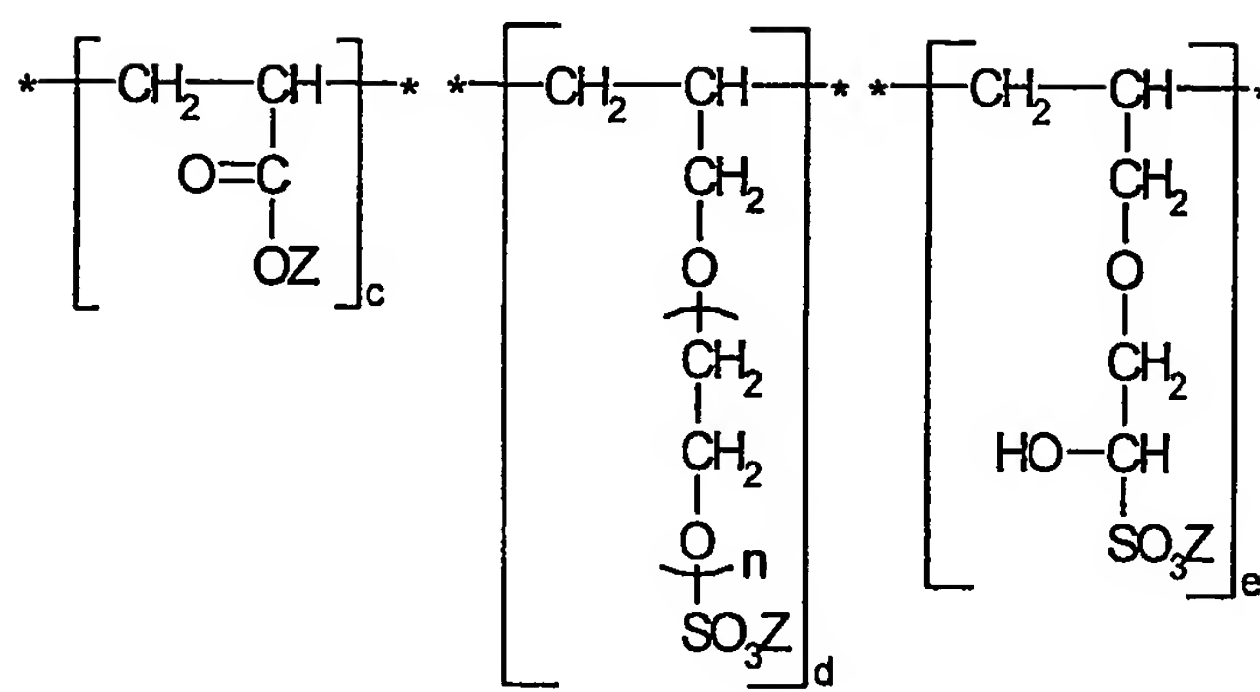
Wherein n is greater than 10. Z is hydrogen or a water-soluble cation such as Na, K, Ca or NH_4 .

Molar ratio c:d ranges from 30:1 to 1:20. Preferably, the molar ratio of c:d ranges from about 15:1 to 1:10. The ratio of c to d is not critical to the present invention providing that the resulting polymer is water-soluble or water-dispersible.

A preferred terpolymer of the present invention, that is where e is a positive integer, is acrylic acid/polyethyleneglycol monoallyl ether sulfate/1-allyloxy-2-hydroxypropylsulfonic acid of the structure.

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Formula IV



10 Wherein n ranges from about 1-100, preferably n is greater than 10. Z is hydrogen or a water-soluble cation such as, Na, K, Ca or NH₄. Z may be the same or different in c, d and e. The mole ratio of c:d:e is not critical so long as the terpolymer is water-soluble or water-dispersible. Preferably the mole ratio c:d:e ranges from about 20:10:1 to 1:1:20.

15 The polymerization of the copolymer and/or terpolymer of the present invention may proceed in accordance with solution, emulsion, micelle or dispersion polymerization techniques. Conventional polymerization initiators such as persulfates, peroxides, and azo type initiators may be used.

Polymerization may also be initiated by radiation or ultraviolet mechanisms.

20 Chain transfer agents such as alcohols, preferably isopropanol or allyl alcohol, amines or mercapto compounds may be used to regulate the molecular weight of the polymer. Branching agents such as methylene bisacrylamide, or polyethylene glycol diacrylate and other multifunctional crosslinking agents may be added.

The resulting polymer may be isolated by precipitation or other well-known techniques. If polymerization is in an aqueous solution, the polymer may simply be used in the aqueous solution form.

The molecular weight of the water-soluble copolymer of Formula I is not
5 critical but preferably falls within the range Mw of about 1,000 to 1,000,000. More preferably from about 1,000 to 50,000 and most preferably from about 1,500 to 25,000. The essential criteria is that the polymer be water-soluble or water-dispersible.

10 USE OF THE POLYMERS

The polymers of the invention are effective for water treatment in cooling water, boiler and steam generating systems as deposit control and/or corrosion inhibition agents. The appropriate treatment concentration will vary depending
15 upon the particular system for which treatment is desired and will be influenced by factors such as the area subjected to corrosion, pH, temperature, water quantity and the respective concentrations in the water of the potential scale and deposit forming species. For the most part, the polymers of the present invention will be effective when used at levels of from about 0.1-500 parts per million parts
20 of water, and preferably from 1 about to 100 parts per million of water contained in the aqueous system to be treated. The polymers may be added directly into the desired water system in an aqueous solution, continuously or intermittently.

The polymers of the present invention are not limited to use in any specific category
25 of aqueous system. They would be expected to inhibit the formation and deposition of scale forming salts in any aqueous system prone to that problem. For instance, in addition to boiler and cooling water systems, the polymers may also be effectively utilized in scrubber systems and the like wherein corrosion and/or the formation and deposition of scale forming salts is a problem. Other
30 possible environments in which the polymers of the present invention may be

used include heat distribution type seawater desalting apparatus, dust collection systems in iron and steel manufacturing industries, mining operations and geothermal systems. The polymers of the present invention are also efficacious as deposit and pitch control agents in the paper and pulp manufacturing processes
5 for preventing deposit of pitch, calcium oxalate and barium sulfate. They can also be used as viscosity modifiers in mining and mineral processing applications to reduce the viscosity of slurries.

The water-soluble or dispersible polymers of the present invention may be used in combination with topping agents in order to enhance the corrosion
10 inhibition and scale controlling properties thereof. For instance, the polymers of the present invention may be used in combination with one or more compounds selected from the group consisting of inorganic phosphoric acids or salts thereof, phosphonic acid salts, organic phosphoric acid esters, and polyvalent metal salts or mixtures thereof. Such topping agents may be added to the system being
15 treated in an amount of from about 1 to 500 ppm.

Examples of inorganic phosphoric acids include condensed phosphoric acids and water-soluble salts thereof. Examples of phosphoric acids include orthophosphoric acids, primary phosphoric acids and secondary phosphoric acids and salts thereof. Examples of inorganic condensed phosphoric acids include
20 polyphosphoric acids such as pyrophosphoric acid, tripolyphosphoric acid and the like, metaphosphoric acids such as trimetaphosphoric acid and tetrametaphosphoric acid and salts thereof.

Examples of other phosphoric acid derivatives, which can be combined with the polymers of the present invention include aminopolyphosphonic acids
25 such as aminotrimethylene phosphonic acid, ethylene diaminetetramethylene phosphonic acid and the like, methylene diphosphonic acid, hydroxyethylidene diphosphonic acid, 2-phosphonobutane 1,2,4, tricarboxylic acid, etc and salts thereof.

Exemplary organic phosphoric acid esters which may be combined with the polymers of the present invention include phosphoric acid esters of alkyl alcohols such as methyl phosphoric acid ester, ethyl phosphoric acid ester, etc., phosphoric acid esters of methyl cellosolve and ethyl cellosolve, and phosphoric acid esters of polyoxyalkylated
5 polyhydroxy compounds obtained by adding ethylene oxide to polyhydroxy compounds such as glycerol, mannitol, sorbitol, etc. Other suitable organic phosphoric esters are the phosphoric acid esters of amino alcohols such as mono, di, and tri-ethanol
10 amines. The water-soluble polymers may also be used in conjunction with molybdates such as, sodium molybdate, potassium molybdate, lithium molybdate, ammonium molybdate, etc.

The polymers of the present invention may be used in combination with
15 yet other topping agents including corrosion inhibitors for iron, steel, copper, and copper alloys or other metals, conventional scale and contamination inhibitors, metal ion sequestering agents, and other conventional water treating agents. Examples of other corrosion inhibitors include tungstate, nitrites, borates, silicates, oxycarboxylic acids, amino acids, catechols, aliphatic amino surface
20 active agents, benzotriazole, halogenated triazoles and mercaptobenzothiazole. Other scale and contamination inhibitors include lignin derivatives, tannic acids, starches, polyacrylic acids and their copolymers including but not limited to acrylic acid/2-acrylamido-2-methylpropanesulfonic acid copolymers and acrylic acid/allyloxy-2-hydroxypropane-3-sulfonic acid copolymers, maleic acids and
25 their copolymers, polyepoxysuccinic acids and polyacrylamides, etc. Examples of metal ion sequestering agents include polyamines, such as ethylene diamine, diethylene triamine and the like and polyamino carboxylic acids, such as nitrilo triacetic acid, ethylene diamine tetraacetic acid, and diethylenetriamine pentaacetic acid.

U.S Patents Nos. 4,659,481; 4,717,499; 4,759,851; 4,913,822; and
4,872,995 disclose the use of specific copolymers in treating cooling, boiler,
steam generating and other aqueous heat transfer systems to inhibit deposition of
scales such as calcium phosphate, calcium phosphonate, calcium oxalate, iron
5 oxide, zinc oxide and silica. Based upon the deposit control efficacy exhibited by
the polymers of the present invention, it is believed that they could be substituted
for the polymers disclosed in the above and other similar patents to provide
improved performance in a wide variety of water based treatment applications.

The copolymers of the present invention can be used alone or in
10 combination with conventional cleaning agents such as surfactants, chelating
agents, citric acid, phosphoric acid and other common reagents to remove deposit
and prevent fouling on membranes used in the micro filtration, ultra filtration and
reverse osmosis applications.

The copolymers of the present invention can also be used as
15 superplasticizers or retarders with cementitious materials in the construction
industry applications. In addition, the polymers of the present invention are
useful as viscosity modifiers to slurry viscosity in the mining and mineral
processing and oil field operations.

The present invention will now be further described with reference to a
20 number of specific examples which are to be regarded solely as illustrative and
not as restricting the scope of the present invention.

EXAMPLES

25 **Example 1**

Preparation of Acrylic Acid/ Ammonium Allylpolyethoxy (10) Sulfate Copolymer

A suitable reaction flask was equipped with a mechanical agitator, a
30 thermometer, a reflux condenser, a nitrogen inlet and two addition inlets for the

initiator and monomer solutions. The flask was charged with 73.5 g of deionized water and 58.5 g (0.1 mol) of ammonium allyl polyethoxy(10) sulfate. While sparging with nitrogen, the solution was heated to 85 °C. An initiator solution containing 2.2 g of 2,2'-azobis(2-amidinopropane) hydrochloride (Wako V-50, from Wako Chemical Company) was sparged with nitrogen for ten minutes. The initiator solution and 21.6 g. (0.3 mol) of acrylic acid were added gradually to the reaction flask over a two-hour period. Following the addition, the solution was heated to 95 °C and held for 90 minutes. The reaction was then cooled to lower than 40 °C and 50% caustic solution was added until the pH measured 8-9. The structure of the resulting copolymer was verified by Carbon 13 NMR. The polymer solution was diluted to 30% solids and had a Brookfield viscosity of 48.6 cps at 25 °C.

Example 2

15 Preparation of Acrylic Acid/ Ammonium Allylpolyethoxy (10) Sulfate Copolymer

Utilizing the procedure and apparatus similar to the prior example, 147 g of deionized water and 61.9 g (0.11 mol) of ammonium allyl polyethoxy(10) sulfate (DVP-010, from Bimax Inc.) were charged to the reaction flask. The solution was heated to 85 °C. An initiator solution containing sodium persulfate 1.9 g in water was sparged with nitrogen for ten minutes. The initiator solution and 22.9 g (0.32 mol) of acrylic acid were gradually added to the reaction flask over a two-hour period. Following the addition, the solution was heated to 95 °C and held for 90 minutes. The reaction was cooled to lower than 40 °C and 50% caustic solution was added until the pH measured 4-5. The structure of the resulting copolymer was verified by Carbon 13 NMR. The polymer solution was diluted to 30% solids and had a Brookfield viscosity of 13.0 cps at 25 °C.

30 Example 3

**Preparation of Acrylic Acid/ Ammonium Allylpolyethoxy (10)
Sulfate/Allyloxy-2-hydroxypropane-3-sulfonic Acid Terpolymer**

Utilizing the procedure and apparatus similar to Example 1, 84.7 g of
5 deionized water, 21.8 g (0.1 mol) of allyloxy-2-hydroxypropane-3-sulfonic acid
and 58.5 g (0.1 mol) of the ammonium allyl polyethoxy-(10)-sulfate monomer
were charged to the reaction flask. While sparging with nitrogen, the solution
was heated to 85 °C. An initiator solution of 2,2'-azobis(2-
10 amidinopropane)hydrochloride and 21.6 g (0.3 mol) of acrylic acid were added to
the reaction flask over a 3.5 hour period. Following the addition, the solution
was heated to 95 °C and held for two hours. The reaction was cooled and a 50%
caustic solution was added for pH adjustment. The structure of the resulting
copolymer was verified by Carbon 13 NMR. The polymer solution was diluted
to 30% solids and had a Brookfield viscosity of 27.2 cps at 25 °C.

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Example 4

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**Preparation of Acrylic Acid/ Methacrylic Acid/Ammonium Allylpolyethoxy
(10) Sulfate Terpolymer**

25 Utilizing the procedure and apparatus similar to Example 1, 109.7 g of
deionized water, 20.6g of isopropyl alcohol and 58.5 g (0.1 mol) of ammonium
allyl polyethoxy-(10)-sulfate monomer mixture were charged to the reaction
flask. While sparging with nitrogen, the solution was heated to 85 °C. A
solution of sodium persulfate and 21.6 g (0.3 mol) of acrylic acid and 8.6 g (0.1
30 mol) of methacrylic acid were added separately to the reaction flask over a two-
hour period. Following the addition, the solution was heated to 95 °C and held
for two hours. After the reaction, isopropyl alcohol was removed from the

solution before cooling down and pH adjustment. The structure of the resulting copolymer was verified by Carbon 13 NMR. The polymer solution was diluted to 25% solids and had a Brookfield viscosity of 21.0 cps at 25 °C.

5 **Example 5**

Preparation of Acrylic Acid/2-Acrylamido-2-methylpropanesulfonic acid /Ammonium Allylpolyethoxy (10) Sulfate Terpolymer

10 Utilizing the procedure and apparatus similar to Example 4, 127.9 g of deionized water, 20.5 g of isopropyl alcohol and 58.5 g (0.1 mol) of ammonium allyl polyethoxy-(10)-sulfate monomer were charged to the reaction flask. While sparging with nitrogen, the solution was heated to 85 °C. Sodium persulfate solution and a solution containing 21.6 g (0.3 mol) of acrylic acid and 20.7 g (0.1
15 mol) of 2-acrylamido-2-methylpropane sulfonic acid (AMPS[®], from Lubrizol Inc.) were added separately to the reaction flask over a two-hour period. Following the addition, the solution was heated to 95 °C and held for two hours before cooling down and pH adjustment. The structure of the resulting copolymer was verified by Carbon 13 NMR. The polymer solution was diluted
20 to 25% solids and had a Brookfield viscosity of 17.0 cps at 25 °C.

Example 6

Preparation of Allylpolyethoxy (10) Phosphate

25 A suitable reaction flask was equipped with a mechanical agitator, a thermometer, and a reflux condenser. 20 g of hydroxypolyethoxy-(10)-allyl ether (0.04 mol., AAE-10, from Bimax Inc.) were charged to the reactor. 6.16 g of phosphorous oxychloride (0.04 mol) was added drop-wise to the reactor. The
30 mixture was stirred vigorously for one hour followed by heating to 50 °C and holding for 4.5 hours. After cooling to ambient temperature, the reaction was

quenched by slow addition to water. The pH was adjusted to 4 with caustic solution. Carbon 13 NMR analysis indicated the presence of phosphate ester.

Example 7

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Preparation of Acrylic Acid/ Allylpolyethoxy (10) Phosphate Copolymer

Utilizing the procedure and apparatus similar to Example 1, 41.3 g of deionized water and 60.3 g (0.05 mol) of 49.8% allylpolyethoxy (10) phosphate from Example 6 were charged to the reaction flask. While sparging with
10 nitrogen, the solution was heated to 85 °C. A solution of 2,2'-azobis(2-amidinopropane)hydrochloride (1.07 g) and 10.7 g (0.147 mol) of acrylic acid were added gradually to the reaction flask over a two-hour period. Following the addition, the solution was heated to 95 °C and held for 90 minutes before cooling
15 down and pH adjustment. The structure of the resulting copolymer was verified by Carbon 13 NMR. The polymer solution was diluted to 25% solids and had a Brookfield viscosity of 221.0 cps at 25 °C.

Example 8

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Preparation of Acrylic Acid/ Allylpolyethoxy (10) Sulfate Copolymer

Utilizing the procedure and apparatus similar to Example 1, 58.6 g of deionized water, 58.6 g (0.1 mol) of allylpolyethoxy (10) sulfate and 0.8 g of allyl alcohol were charged to the reaction flask. While sparging with nitrogen,
25 the solution was heated to 85 °C. A solution of sodium persulfate (1.92 g) in 6.0 g of water and 21.6 g (0.147 mol) of acrylic acid were added gradually to the reaction flask over a two-hour period. Following the addition, the solution was heated to 95 °C and held for 90 minutes before cooling down and pH adjustment. The structure of the resulting copolymer was verified by Carbon 13 NMR. The
30 polymer solution was diluted to 25% solids and had a Brookfield viscosity of 65.0 cps at 25 °C.

Table 1 summarizes the composition and physical properties of the copolymers prepared in accordance to the procedure described above. In Table 1, Examples 1-8 were prepared in accordance with the above correspondingly numbered descriptions. Example 9 was prepared in accordance with the description above for Examples 3-5 with a modified comonomer molar ratio. Examples 10-20 were prepared in accordance with the descriptions of Examples 1 and 2 with modified comonomer molar ratios and molecular weights. The molecular weights were obtained by Size Exclusion Chromatography analysis using polyacrylic acid as standards.

TABLE I

Example	Polymer Composition Comonomer Molar Ratio	% Solids	Brookfield Viscosity #1 S @60 rpm	pH	Molecular Weight (Mw)
1	AA/APES (3/1)	29.70	48.6	9.8	18,420
2	AA/APES (3/1)	29.23	13.0	4.2	30,670
3	AA/AHPS/APES (3/1/1)	30.10	27.2	8.3	13,100
4	AA/MAA/APES (3/1/1)	25.20	21.0	5.7	19,600
5	AA/AMPS/APES (3/1/1)	25.10	17.0	5.8	17,800
6	AA/AAE-10 phosphate (3/1)	25.7	221.0	6.5	-
7	MAA/APES (6/1)	30.75	44.3	8.3	11,490
8	AA/APES (3/1)	25.7	65.0	7.4	72,100
9	AA/AHPS/APES (6/1/1)	30.47	30.5	9.4	15,790
10	AA/AHPS/APES (3/1/1)	30.11	28.3	8.0	8,252
11	AA/APES (3/1)	29.53	13.2	4.4	13,100
12	AA/APES (3/1)	25.10	19.0	6.1	15,300
13	AA/APES (3/1)	24.8	13.0	5.9	10,100
14	AA/APES (3/1)	29.46	19.6	5.9	5,910
15	AA/APES (4/1)	30.76	18.5	5.9	4,660
16	AA/APES (4/1)	24.9	16.0	6.0	12,600
17	AA/APES (4/1)	25.16	15.0	4.1	43,700
18	AA/APES (6/1)	24.10	20.0	6.0	14,200
19	AA/APES (6/1)	27.15	42.4	4.1	138,090
20	AA/APES (6/1)	30.13	15.2	4.1	5,250

AA = acrylic acid

MAA = methacrylic acid

APES = ammonium allylpolyethoxy(10) sulfate, containing 10 moles of ethylene oxide, DVP-010, from Bimax Inc.

AHPS = 1-allyloxy-2-hydroxypropyl-3-sulfonic ether, from BetzDearborn Inc.

5 AAE-10 Phosphate = polyethyleneglycol (10 moles of ethylene oxide) allyl ether phosphate

AMPS[®] = 2-acrylamido-2-methylpropanesulfonic acid, from Lubrizol Inc.

10 Example 9

Phosphate Scale Inhibition – Bottle Test Protocol

The testing of phosphate scale inhibition was undertaken in a static beaker
 15 test at varying treatment levels. The test protocol involved adding the treatment to a 100 ml solution containing calcium and phosphate ions and having a pH of 8.2 at 70° C. After 18 hours, a portion was filtered hot and the pH adjusted to <2.0 with hydrochloric acid. Percent inhibition was calculated from the determination of phosphate concentrations in the treated, stock and control
 20 solutions. The solution appearance was evaluated by visual inspection and compared to stock solutions. The conditions of the tests were: 400 ppm Ca, 100 ppm Mg and 35 ppm M-alkalinity all as CaCO₃. Table 2 summarizes the percent inhibition of a known polymeric inhibitor/dispersant and polymers in accordance with the present invention over a broad range of treatment dosages. Table 3
 25 summarizes the percent inhibition of a known polymeric inhibitor/dispersant and polymers in accordance with the present invention over a broad range of treatment dosages in the presence of 3 ppm FeCl₂. The data in tables 2 and 3 show the efficacy of the polymeric treatments of the present invention compared to a known treatment.

30

Table 2: Percent Inhibition of various polymeric inhibitors/dispersants.

Treatm nt	5 ppm	7.5 ppm	10 ppm	12 ppm
AA/AHPS	16.5	12	36.5	97
AA/AHPS/APES (3/1/1)	75	90	96.5	97.5

AA/APES (3/1)	59.7	100	96.5	96.7
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AA/AHPS is Acrylic acid/Allyl hydroxypropyl sulfonate ether, Mw about 15,000.

AA/AHPS /APES is Acrylic acid/Allyl hydroxypropyl sulfonate ether/Allylpolyethoxy sulfate prepared in accordance with Example 3 above.

AA/APES is Acrylic acid/ Allylpolyethoxy sulfate prepared in accordance with Example 1 above.

Table 3: Percent Inhibition of various polymeric inhibitors/dispersants in the presence of 3 ppm of FeCl₂.

Treatment	5 ppm	7.5 ppm	10 ppm	12 ppm
AA/AHPS	0	3.3	77.8	100
AA/AHPS/APES (3/1/1)	25.5	80.5	100	100
AA/APES (3/1)	56.6	100	100	100

AA/AHPS is Acrylic acid/Allyl hydroxypropyl sulfonate ether, Mw about 15,000.

AA/AHPS /APES is Acrylic acid/Allyl hydroxypropyl sulfonate ether/Allylpolyethoxy sulfate prepared in accordance with Example 3 above.

AA/APES is Acrylic acid/ Allylpolyethoxy sulfate prepared in accordance with Example 1 above.

Example 10

Phosphate Scale Inhibition – Dynamic Heat Transfer Simulations

Developmental testing was also initiated with the AA/APES (3:1), Mw about 18,000, chemistry under dynamic heat transfer conditions in a laboratory scale cooling test rig. The water matrix contained 600 ppm Ca, 300 ppm Mg, 50 ppm M-alkalinity (all as CaCO₃), 15 ppm orthophosphate, 3 ppm pyrophosphate, 1.2 ppm halogen substituted azole corrosion inhibitor, and either the AA/APES (Mw about 18,000), AA/AHPS (Mw about 15,000) or AA/AHPS/APES (Mw about 13,000) polymer. Operating parameters included a bulk temperature of 120⁰ F, a heat transfer rate of 8,000 BTU/(ft²*hr) across a mild steel heat transfer tube, a water velocity of 2.8 ft/sec, a retention time of 1.4 days (to 75% depletion) and a test duration of 7 days. Both mild steel and admiralty brass coupons were also inserted into the test rig. A summary of the polymer comparison is shown below.

	Dosage (ppm)	Turbidity (NTU)	Delta PO4 (ppm)	Heat Transfer Appearance
AA/AHPS	4	0.68	0.23	Fail - <i>Slight Deposition</i>
AA/AHPS	5	0.36	0.2	Pass - <i>Very Slight Deposition</i>
AA/APES	2	0.15	0.2	Pass - <i>No Deposition</i>

In this simulation, three parameters are monitored which are indicative of polymer performance. They are 1) the bulk turbidity values which develop in the cooling water, 2) the average delta phosphate values (the difference between filtered and unfiltered phosphate concentrations), and 3) the amount of deposition which is observed on the heat transfer tube. Under this recirculating rig condition, 5 ppm AA/AHPS is necessary to maintain acceptable heat transfer deposit control. A lower dosage of 4 ppm AA/AHPS results in a failure as indicated by slight deposition having been observed on the tube surface. In contrast, 2 ppm of the AA/APES chemistry not only keeps bulk turbidity and delta phosphate values low but also keeps the heat transfer surface free of deposition. This is a significant reduction (60%) in the amount of polymer necessary to control deposition in this cooling water.

Additional testing was conducted under two upset conditions, i.e. elevated temperature/heat flux and 3 ppm iron contamination. These results are shown below.

	Dosage (ppm)	Turbidity (ntu)	Delta PO4 (ppm)	Heat Transfer Appearance
<i>High Temp/Flux</i> AA/AHPS	5	0.33	0.2	Fail - <i>Slight Deposition</i>
AA/APES	2	0.31	0.5	Pass - <i>Very Slight Deposition</i>
<i>3 ppm Fe+2</i> AA/AHPS	12	7.1	1.2	Fail - <i>Slight Deposition</i>
AA/AHPS	9	12.9	3.7	Fail - <i>Slight Deposition</i>
AA/APES	6	5.3	0.6	Pass - <i>No Deposition</i>

The high temperature/flux evaluations were conducted using a bulk temperature of 140⁰ F and a heat flux of 16,000 BTU/(ft²*hr) across the mild steel heat transfer tube. Again, the AA/AHPS simulation, at a dosage of 5 ppm, resulted in a test failure with significant heat transfer deposition having been
5 observed. During the 2 ppm AA/APES evaluation, only a very slight amount of deposit was observed under this stressed condition.

The iron contamination studies were conducted by adding 0.5 ppm iron (Fe⁺²) to the cooling water after the initial 24 hours of the evaluation. At this point, continuous feed of an iron solution was initiated into the test rig targeting a
10 3 ppm iron level, i.e. a 100 ppm Fe⁺² solution was now fed to the rig at a rate of 0.24 mls/min. Under this condition, AA/AHPS was shown to be ineffective at both a 9 ppm and a 12 ppm dosage. Elevated turbidity (7-13 NTU) and delta phosphate values (1-3.7 ppm) were observed, in addition to unacceptable deposition having formed on the heat transfer surface. The AA/APES chemistry,
15 at a lower dosage of 6 ppm, maintained a lower bulk turbidity (5.3 ntu), a lower delta phosphate value (0.6 ppm) and, most importantly, prevented deposition on the heat transfer tube surface.

Example 11

20 Silica Polymerization Inhibition

Testing of silica polymerization inhibition was undertaken. The testing involved preparing 100 ml of a 500 ppm silica solution adjusted to pH 7.4, and adding 30 ppm of a treatment. This solution was placed in a 30° C water bath and
25 monomeric silica determinations were initiated and repeated every 30 minutes. The Hach Molybdate Reactive Silica test was utilized to determine the polymerization of silica. As polymerization occurs, the monomeric silica levels decrease. If the treatment is effective, elevated monomeric concentrations are realized relative to the untreated control. Tables 4 and 5 summarize the results of

testing of several conventional treatments as well as a polymer in accordance with the present invention. At each time interval, the AA/APES chemistry maintains higher monomeric silica levels i.e. inhibits polymerization, than the other treatments.

5

10 **Table 4 : Silica Levels (ppm) as a function of time (minutes) for each treatment**

Time	Control	AA/AHPS Mw about 18,000	AA/PEG Mw~35,000	AA/AHPS/PEG Mw~25-28,000	Dequest 2010	AA/AHPS Mw about 13,000
0	430	460	470	485	492	
30	390	380	408	438	458	463
60	368	325	355	400	412	395
90	325	302	322	358	368	343
120	300	288	312	328	342	318
150	278	278	290	318	328	298
180	275	262	280	295	308	275
210	260	258	270	282	300	290
240	242	240	242	268	270	258
270	230	245	260	270	268	253
300	235	242	262	255	268	243
330	222	238	242	248	260	238
360	230	242	242	245	255	230
390	225	215	230	230	248	225

PEG is polyethyleneglycol (10 moles of ethyleneoxide) allyl ether

15 **Table 5 : Silica Levels (ppm) as a function of time (minutes) for each treatment**

Time	Control	Acumer 1100	AA/AEPS Mw about 18,000	Belclene 400	PESA
0	430	530	495	483	495
30	390	368	458	400	463
60	368	320	468	365	445

90	325	273	450	325	420
120	300	263	433	310	385
150	278	250	425	283	363
180	275	240	418	275	348
210	260	248	388	265	325
240	242	232	388	255	302
270	230	228	375	255	282
300	235	220	362	240	280
330	222	222	345	235	270
360	230	213	343	238	265
390	225	215	332	232	252

Acumer 1100 is polyacrylic acid available from Rohm & Haas.

Belclene 400 is available from FMC Corp.

PESA is polyepoxysuccinic acid

5 Example 12

Silica Deposition Inhibition

Bottle tests were conducted to evaluate the effects of treatments of the present invention on the solubility of silica and phosphate in the presence of aluminum.

The test waters contained 700 ppm calcium, 185 ppm magnesium and 35 ppm M
 10 Alkalinity (all as CaCO_3), 90 ppm SiO_2 , 14 ppm orthophosphate, 2 ppm
 pyrophosphate + a specific treatment. Treatments included a copolymer of
 AA/AHPS (Mw about 15,000), a second copolymer of AA/AHPS with a higher
 molecular weight (Mw about 55,000), and HEDP (hydroxyethylidene
 diphosphonic acid). The test waters were placed in 100 ml aliquots. A dosage of
 15 5.0 ppm Al^{3+} was added to each aliquot, the pH adjusted to 8.0 and the aliquots
 held at 130 °F overnight. Filtered/unfiltered (F/UF) analyses of the water
 constituents were then conducted. The following table shows the results.

Treatment, ppm	Al (F/UF)	Mg (F/UF)	TP (F/UF)	SiO_2 (F/UF)	Ca (F/UF)
AA/AHPS-1, 20	0.1/5.1	190/190	6.5/16	71/89	680/700
AA/AHPS-1, 35	0.8/5.1	180/190	8.9/16	71/88	670/690
AA/AHPS-1, 50	2.0/5.0	180/190	11/16	75/88	670/690
AA/AHPS-2, 20	0.2/5.0	190/190	6.2/15	71/88	670/690
AA/AHPS-2, 35	0.8/5.1	190/190	8.5/16	73/89	690/700
AA/AHPS-2, 50	2.8/5.1	190/190	15/15	79/88	680/700

AA/AHPS-2, 20 + HEDP, 1.7	0.2/5.1	190/190	6.1/17	71/90	680/710
AA/AHPS-2, 35 + HEDP, 3.0	0.7/5.1	190/190	9.6/19	73/89	690/700
AA/AHPS-2, 50 + HEDP, 4.3	1.0/4.9	190/180	12/19	73/86	680/680
AA/APES, 20	4.0/5.1	190/190	13/15	83/88	690/690
AA/APES, 35	4.8/5.1	190/190	15/15	87/90	700/710
AA/APES, 50	5.0/5.0	190/180	15/14	88/87	700/680

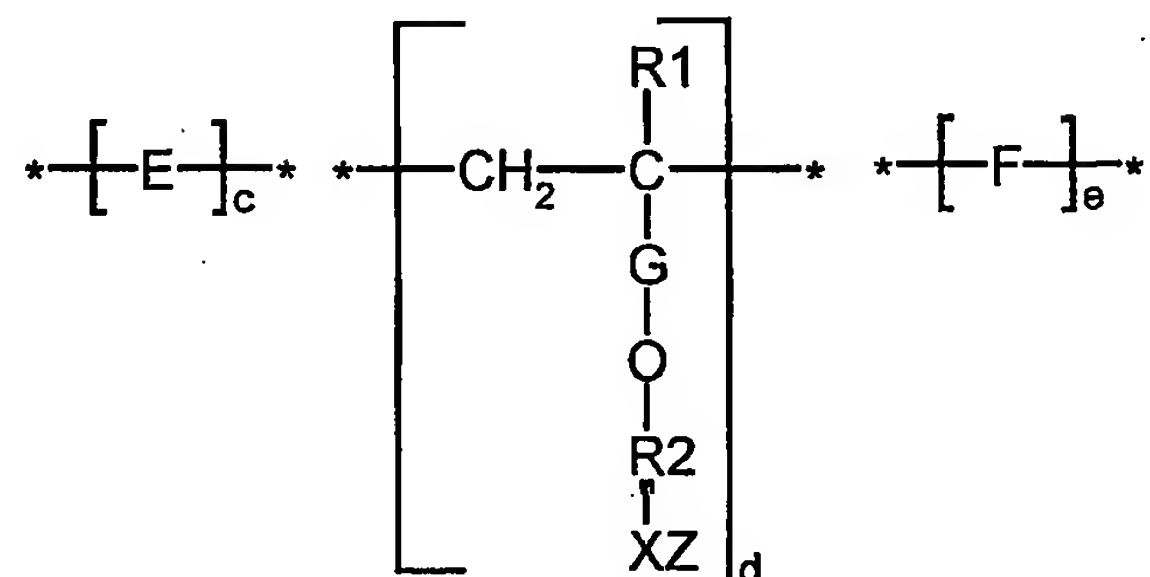
As the table shows, AA/AHPS 1 (Mw about 15,000), AA/AHPS-2 (Mw about 55,000), and AA/AHPS-2 + HEDP, were ineffective in maintaining solubility, even at very high dosages. In striking contrast, the AA/APES (Mw about 13,000) polymer kept all the species soluble, even when fed at lower dosages.

While this invention has been described with respect to particular embodiments thereof, it is apparent that numerous other forms and modifications of this invention will be obvious to those skilled in the art. The appended claims and this invention generally should be construed to cover all such obvious forms and modifications which are within the true spirit and scope of the present invention.

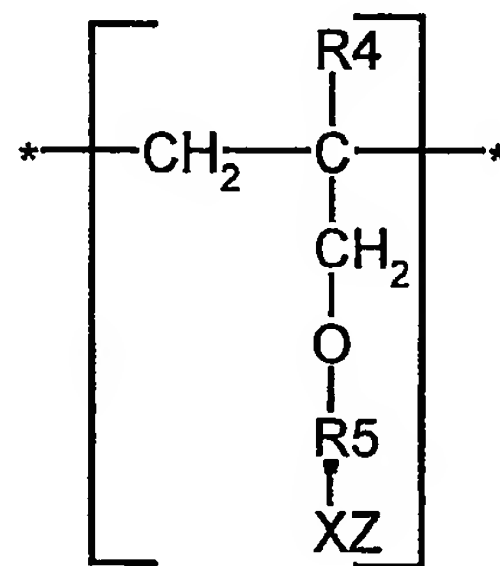
What is Claimed is:

1. A composition comprising a water-soluble or water dispersible polymer of the formula:

5



- 10 wherein E is the repeat unit remaining after polymerization of an ethylenically unsaturated compound; R₁ is H or lower (C₁-C₄) alkyl; G is -CH₂- or -CHCH₃-; R₂ is
 -(CH₂-CH₂-O)_n or -(CH₂-CHCH₃-O)_m;
 15 wherein n and m range from about 1 to 100; X is SO₃, PO₃ or COO; Z is H, hydrogens, or a water soluble cationic moiety; F is a repeat unit of the formula:



20

wherein R_4 is H or lower (C_1 - C_4) alkyl, R_5 is hydroxy substituted alkyl or alkylene having from 1 to 6 carbon atoms; c and d are positive integers; and e is a non-negative integer.

5 2. The composition of claim 1, wherein said ethylenically unsaturated compound is one or more of: carboxylic acid, sulfonic acid, phosphonic acid or amide form thereof or mixtures thereof.

10 3. The polymer of claim 2, wherein said ethylenically unsaturated compound is one or more of: acrylic acid, methacrylic acid, acrylamide, methacrylamide, N-methyl acrylamide, N, N-dimethyl acrylamide, N-isopropyl acrylamide, maleic acid or anhydride, fumaric acid, itaconic acid, styrene sulfonic acid, vinyl sulfonic acid, isopropenyl phosphonic acid, vinyl phosphonic acid, vinylidene diphosphonic acid, 2-acrylamido-2-methylpropane sulfonic acid or
15 mixtures thereof.

4. The composition of claim 1, wherein said water soluble cationic moiety is selected from the group Na, K, Ca or NH_4 .

20 5. The composition of claim 1, wherein the molecular weight Mw ranges from 1,000–1,000,000.

6. The composition of claim 1, wherein the molecular weight Mw ranges from about 1,000 to about 50,000.

25

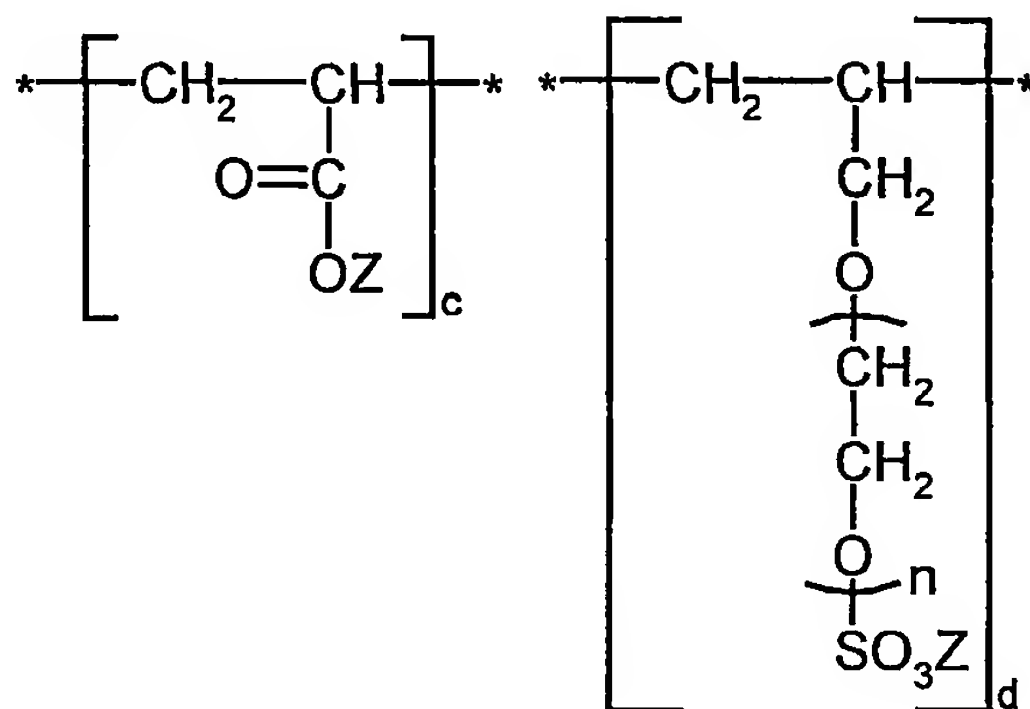
7. The composition of claim 1, wherein the molecular weight Mw ranges from about 1,500 to 25,000.

8. The composition of claim 1, wherein the ratio c:d:e ranges from about 20:10:1 to 1:1:20.

9. The composition of claim 1, wherein e is zero and the ration c:d
5 ranges from about 30:1 to about 1:20.

10. The composition of claim 1, wherein n is greater than 10.

11. A composition comprising a water-soluble or water dispersible
10 polymer of the formula:



15 wherein n ranges from about 1-100, Z is hydrogen or a water soluble cation.

12. The composition of claim 11, wherein said water soluble cation is selected form the group consisting of Na, K, Ca or NH₄ or mixtures thereof.

20

13. The composition of claim 11, wherein the ratio c:d ranges from about 30:1 to about 1:20.

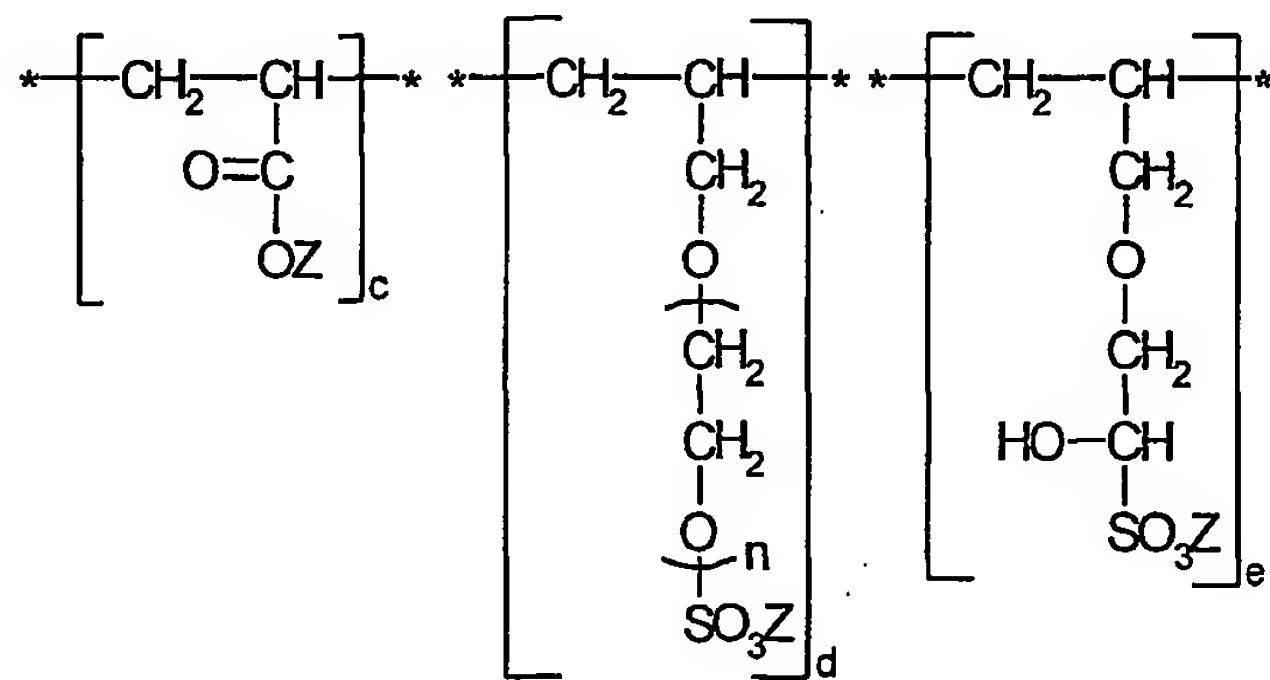
14. The composition of claim 11, wherein the molecular weight Mw ranges from about 1,000 to 1,000,000.

15. The composition of claim 11, wherein the molecular weight Mw ranges from about 1,000 to 50,000.

16. The composition of claim 11, wherein the molecular weight Mw ranges from about 1,000 to 25,000.

17. The composition of claim 11, wherein n is greater than 10.

18. A composition comprising a water-soluble or water dispersible polymer of the formula:



wherein n ranges from about 1-100, and Z is hydrogen or a water soluble cation.

19. The composition of claim 18, wherein said water soluble cation is selected from the group consisting of Na, K, Ca or NH₄ or mixtures thereof.

20. The composition of claim 18, wherein the ration c:d:e ranges from about 20:10:1 to about 1:1:20.

21. The composition of claim 18, wherein the molecular weight Mw ranges from about 1,000 to 1,000,000.

5 22. The composition of claim 18, wherein the molecular weight Mw ranges from about 1,000 to 50,000.

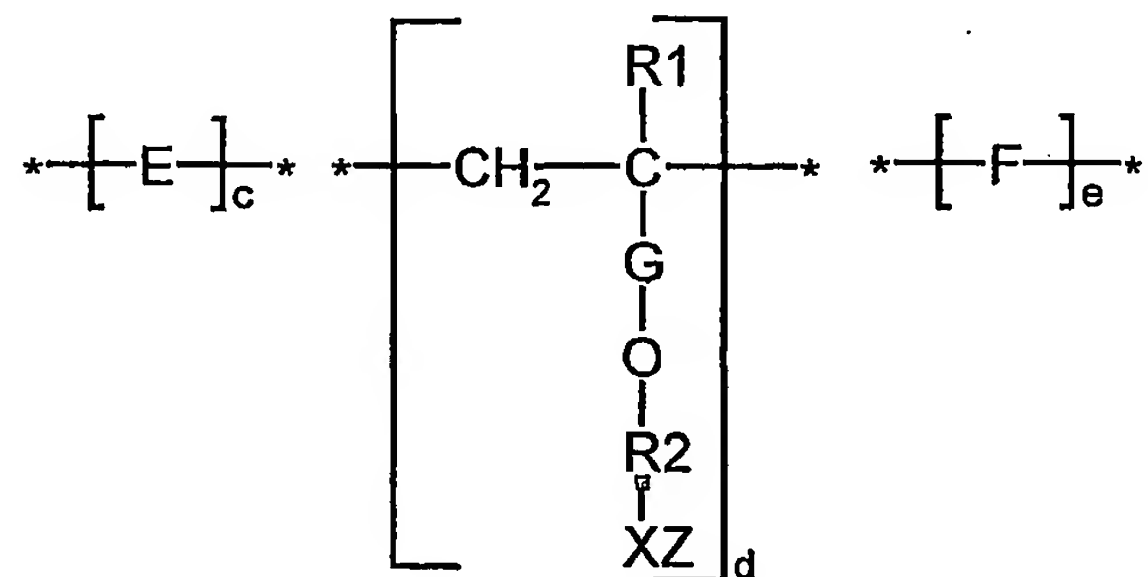
23. The composition of claim 18, wherein the molecular weight Mw ranges from about 1,000 to 25,000.

10

24. The composition of claim 18, wherein n is greater than 10.

25. A method of inhibiting the formation and deposition of scale
15 imparting species on surfaces exposed to an aqueous system comprising adding to said aqueous system an effective amount for the purpose of a water-soluble or water- dispersible polymer of the formula:

20



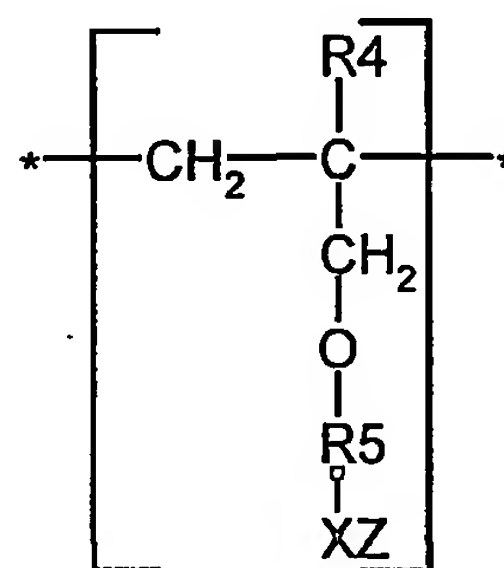
wherein E is the repeat unit remaining after polymerization of an ethylenically unsaturated compound; R₁ is H or lower (C₁-C₄) alkyl; G is -CH₂- or -CHCH₃-;

25 R₂ is

$\text{-(CH}_2\text{-CH}_2\text{-O)-}_n$ or $\text{-(CH}_2\text{-CHCH}_3\text{-O)-}_m$;

wherein n and m range from about 1 to 100; X is SO₃, PO₃ or COO; Z is H, hydrogens, or a water-soluble cationic moiety; F is a repeat unit of the formula:

5



wherein R₄ is H or lower (C₁-C₄) alkyl, R₅ is hydroxy substituted alkyl or alkylene having from 1 to 6 carbon atoms; c and d are positive integers; and e is a non-negative integer.

10

26. The method of claim 25, wherein said ethylenically unsaturated compound is one or more of: carboxylic acid, sulfonic acid, phosphonic acid or amide form thereof or mixtures thereof.

15

27. The method of claim 26, wherein said ethylenically unsaturated compound is one or more of: acrylic acid, methacrylic acid, acrylamide, methacrylamide, N-methyl acrylamide, N, N-dimethyl acrylamide, N-isopropyl acrylamide, maleic acid or anhydride, fumaric acid, itaconic acid, styrene sulfonic acid, vinyl sulfonic acid, isopropenyl phosphonic acid, vinyl phosphonic acid, vinylidene diphosphonic acid, 2-acrylamido-2-methylpropane sulfonic acid or mixtures thereof.

20

28. The method of claim 25, wherein said water-soluble cationic moiety is selected from the group Na, K, Ca or NH₄.

25

29. The method of claim 25, wherein the molecular weight Mw ranges from 1,000–1,000,000.

5 30. The method of claim 25, wherein the molecular weight Mw ranges from about 1,000 to about 50,000.

31. The method of claim 25, wherein the molecular weight Mw ranges from about 1,500 to 25,000.

10

32. The method of claim 25, wherein the ratio c:d:e ranges from about 20:10:1 to 1:1:20.

33. The method of claim 25, wherein e is zero and the ration c:d
15 ranges from about 30:1 to about 1:20.

34. The method of claim 25, wherein n is greater than 10.

35. The method of claim 1, wherein said polymer is added to said
20 aqueous system in an amount from about 0.1 ppm to about 500 ppm.

36. The method of claim 25, wherein said polymer is added to said aqueous system in an amount of from about 1 ppm to about 100 ppm.

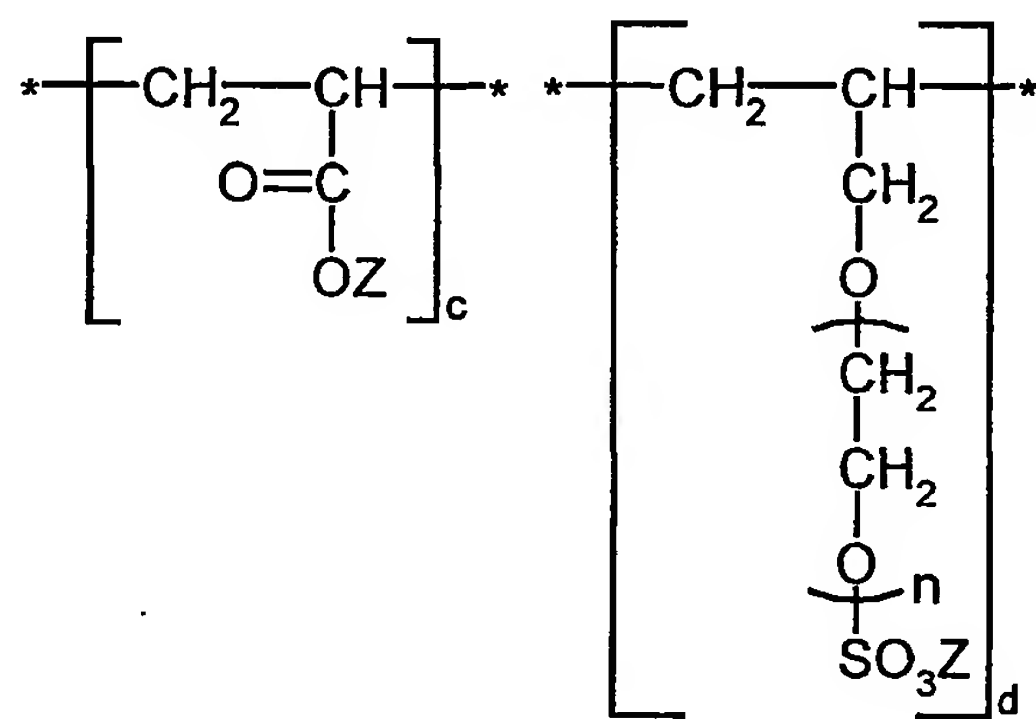
25 37. The method of claim 25, where in said aqueous system is a steam generating system.

38. The method of claim 25, wherein said aqueous system is a cooling water system.

39. The method of claim 25, wherein said aqueous system is a gas scrubber system.

5 40. The method of claim 25, wherein said water-soluble or water-dispersible polymer is added in combination with at least one or more topping agents.

41. A method of inhibiting the formation and deposition of scale
10 imparting species on surfaces exposed to an aqueous system comprising adding to said aqueous system an effective amount for the purpose of a water-soluble or water-dispersible polymer of the formula:



15

wherein n ranges from about 1-100, Z is hydrogen or a water-soluble cation.

20 42. The method of claim 41, wherein said water soluble cation is selected from the group consisting of Na, K, Ca or NH₄ or mixtures thereof.

43. The method of claim 41, wherein the ratio c:d ranges from about 30:1 to about 1:20.

44. The method of claim 41, wherein the molecular weight Mw ranges
5 from about 1,000 to 1,000,000.

45. The method of claim 41, wherein the molecular weight Mw ranges from about 1,000 to 50,000.

10 46. The method of claim 41, wherein the molecular weight Mw ranges from about 1,000 to 25,000.

47. The method of claim 41, wherein n is greater than 10.

15 48. The method of claim 41, wherein said polymer is added to said aqueous system in an amount from about 0.1 ppm to about 500 ppm.

49. The method of claim 41, wherein said polymer is added to said aqueous system in an amount of from about 1 ppm to about 100 ppm.

20

50. The method of claim 41, where in said aqueous system is a steam generating system.

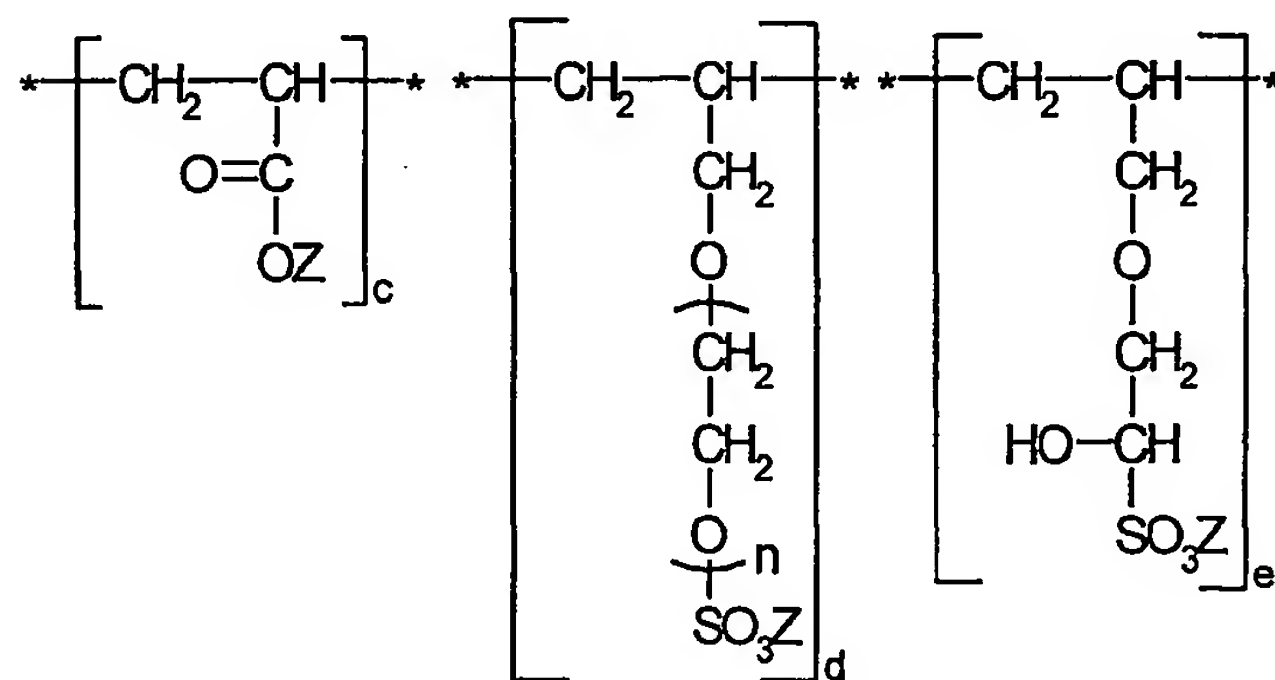
51. The method of claim 41, wherein said aqueous system is a cooling
25 water system.

52. The method of claim 41, wherein said aqueous system is a gas scrubber system.

53. The method of claim 41, wherein said water-soluble or water-dispersible polymer is added in combination with at least one or more topping agents.

5

54. A method of inhibiting the formation and deposition of scale imparting species on surfaces exposed to an aqueous system comprising adding to said aqueous system an effective amount for the purpose of a water-soluble or water-dispersible polymer of the formula:



10

wherein n ranges from about 1-100, and Z is hydrogen or a water-soluble cation.

55. The method of claim 54, wherein said water soluble cation is
15 selected from the group consisting of Na, K, Ca or NH₄ or mixtures thereof.

56. The method of claim 54, wherein the ration c:d:e ranges from
about 20:10:1 to about 1:1:20.

20 57. The method of claim 54, wherein said polymer is added to said
aqueous system in an amount from about 0.1 ppm to about 500 ppm.

58. The method of claim 54, wherein said polymer is added to said aqueous system in an amount of from about 1 ppm to about 100 ppm.

59. The method of claim 54, wherein said aqueous system is a steam
5 generating system.

60. The method of claim 54, wherein said aqueous system is a cooling water system.

10 61. The method of claim 54 wherein said aqueous system is a gas scrubber system.

62. The method of claim 54, wherein the molecular weight Mw ranges
15 from about 1,000 to 1,000,000.

63. The method of claim 54, wherein the molecular weight Mw ranges from about 1,000 to 50,000.

20 64. The method of claim 54, wherein the molecular weight Mw ranges from about 1,000 to 25,000.

65. The method of claim 54, wherein n is greater than 10.

25 66. The method of claim 54, wherein said water-soluble or water-dispersible polymer is added in combination with at least one or more topping agents.

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 02/06370

A. CLASSIFICATION OF SUBJECT MATTER
 IPC 7 C02F5/10 C08F216/14

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 C02F C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, CHEM ABS Data, COMPENDEX

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 5 575 920 A (FREESE DONALD T ET AL) 19 November 1996 (1996-11-19) cited in the application the whole document	1-66
Y	US 4 500 693 A (TAKEHARA HIDETOSHI ET AL) 19 February 1985 (1985-02-19) the whole document	1-66
X	US 3 875 202 A (STECKLER ROBERT) 1 April 1975 (1975-04-01) cited in the application the whole document	1,4,5,9, 10
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